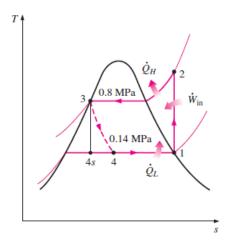
Example 11

A refrigerator uses refrigerant-134a as working fluid and operates on an ideal vapor-compression refrigeration cycle between 0.14 and 0.8 MPa. If the mass flow rate of the refrigerant is 0.05 kg/s, determine (a) rate of heat removal from the refrigerated space and the power input to the compressor, (b) rate of heat rejection to the environment, and (c) COP of the refrigerator.



This is an ideal vapor-compression refrigeration cycle, and thus

- compressor is isentropic and the refrigerant leaves the condenser as a saturated liquid
- enters the compressor as saturated vapor

From the refrigerant-134a tables, enthalpies are determined as follows:

$$\begin{split} P_1 &= 0.14 \text{MPa} \Rightarrow h_1 = h_{g@0.14\text{MPa}} = 239.16 \text{kJ} / \text{kg} \\ &s_1 = s_{g@0.14\text{MPa}} = 0.94456 \text{kJ} / \text{kgK} \\ P_2 &= 0.8 \text{MPa} \Rightarrow s_2 = s_1 = 0.94456 \text{kJ} / \text{kgK} \\ &h_2 = 275.39 \text{kJ} / \text{kg} \\ \end{split}$$

$$P_3 &= 0.8 \text{ MPa} \Rightarrow h_3 = h_{f@0.8\text{MPa}} = 95.47 \text{ kJ} / \text{kg} \end{split}$$

$$h_4 \approx h_3$$
 (throttling valve) $\Rightarrow h_4 = 95.47 \text{ kJ} / \text{kg}$

a) Rate of heat removal from refrigerated space and the power input to compressor;

$$\dot{Q}_{L} = \dot{m} (h_{1} - h_{4}) = 0.05 [(239.16 - 95.47) kJ / kg] = 7.18 kW$$

 $\dot{W}_{in} = \dot{m} (h_{2} - h_{1}) = 0.05 [(275.39 - 239.16) kJ / kg] = 1.81 kW$

b) Rate of heat rejection from the refrigerant to the environment

$$\dot{Q}_{H} = \dot{m} (h_{2} - h_{3}) = 0.05 \text{ kg} / \text{s}231275.39 95.472 \text{ kJ} / \text{kg} = 9.0 \text{ kW}$$

It could also be determined from,

$$\dot{Q}_{\rm H} = \dot{Q}_{\rm L} + \dot{W}_{\rm in} = 7.18 + 1.81 = 8.99 \, \rm kW$$

c) Coefficient of performance of the refrigerator is,

$$\text{COP}_{\text{R}} = \frac{\dot{\text{Q}}_{\text{L}}}{\dot{\text{W}}_{\text{in}}} = \frac{7.18 \text{ kW}}{1.81 \text{ kW}} = 3.97$$

d) It would be interesting to see what happens if the throttling valve were replaced by an isentropic turbine.

At
$$P_{4s} = 0.14$$
 MPa
 $s_{4s} = s_3 = 0.35404$ kJ/kg · K
 $s = s_f + xs_{fg}$
 $0.35404 = 0.11087 + x(0.83368)$
 $x = 0.2917$
 $h = h_f + xh_{fg}$
 $= 27.08 + 0.2917(212.08)$
 $\Rightarrow h_{4s} = 88.94$ kJ/kg
 $W_{turbine} = \dot{m} (h_3 - h_{4s}) = 0.05 (95.47 - 88.94) = 0.33$ kW

Turbine would produce 0.33 kW of power.

It would increase the rate of heatremoval from the refrigerated space from 7.18 to 7.51 kW.

$$\dot{Q}_{L} = \dot{m} (h_{1} - h_{4s}) = (0.05 \text{ kg/s})[(239.16 - 88.94) \text{ kJ/kg}] = 7.51 \text{ kW}$$
$$\dot{W}_{in} = 1.81 - 0.3265 = 1.48 \text{ kW}$$
$$COP_{R} = \frac{\dot{Q}_{L}}{\dot{W}_{in}} = \frac{7.51 \text{ kW}}{1.48 \text{ kW}} = 5.07$$

As a result, the COP of the refrigerabr would increase from 3.97 to 5.07, an increase of 28 percent.