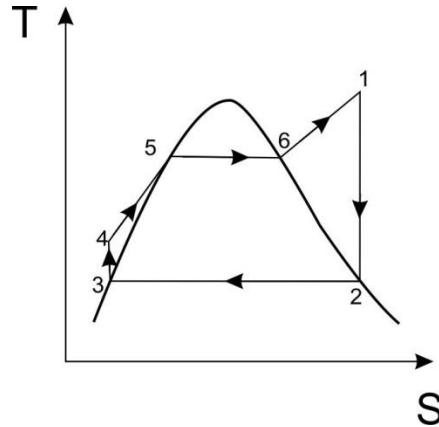


Example 2

Compare the Rankine cycle performance of example 1 with that obtained when steam is superheated to 500°C. Neglect the feed pump work.



$$h_{1@42\text{bar}} = 34427 \text{ kJ/kg}$$

$$s_{1@42\text{bar}} = 7.069 \text{ kJ/kg}$$

$$s_2 = s_{f2} + x_2 s_{fg2}$$

$$7.069 = 0.391 + x_2 8.13$$

$$x_2 = 0.821$$

$$h_2 = h_{f2} + x_2 h_{fg2}$$

$$= 111.8 + (0.821 \times 2438.53) = 2114.81 \text{ kJ/kg}$$

$$h_3 = 111.8 \text{ kJ/kg}$$

$$W_{12} = h_1 - h_2 = 34427 - 2114.81 = 1327.89 \text{ kJ/kg}$$

Neglecting feed pump

$$Q_{in} = h_1 - h_3 = 33309 \text{ kJ/kg}$$

$$\eta = \frac{h_1 - h_2}{h_1 - h_3} = \frac{34427 - 2114.81}{34427 - 111.8} = \frac{1327.89}{33309} = 0.399 @ 39.9\%$$

The thermal efficiency has increase due to superheating and improvement in SCC

$$SSC = \frac{3600}{W_{12}} = \frac{3600}{1327.89} = 2.71 \text{ kg/kWhr}$$

The condenser heat loads for different plants can be compared by calculating the rate of heat removal in the condenser, per unit power output.

$$\text{Condenser heat load} = \text{ssc} \times (h_2 - h_3)$$

With dry saturated steam at entry of turbine

$$\text{Condenser heat load} = 3.64(1808 - 112) = 6175(\text{kJ/h})/\text{kW}$$

With superheated steam at entry of turbine

$$\text{Condenser heat load} = 2.71(2113 - 112) = 5420(\text{kJ/h})/\text{kW}$$

