

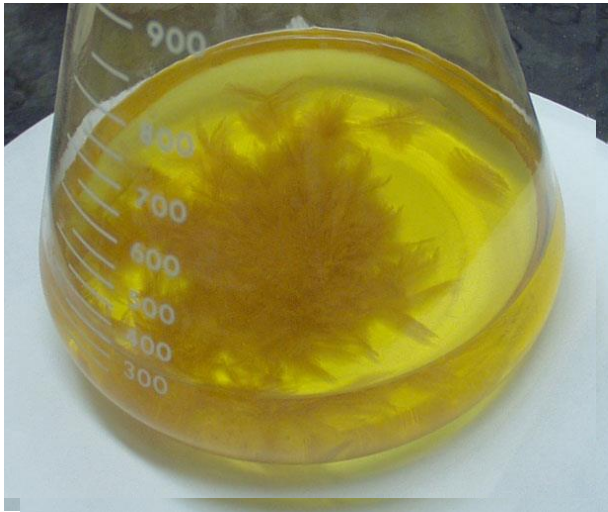
# CRYSTALLIZATION

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- **important industrially because:**

- i) a crystal formed from an impure solution and itself pure**

- ii) Practical method of obtaining pure chemical substances in a satisfactory condition for packaging and storing**



- **solid-liquid separation process**

- **yield , purity, sizes & shapes of crystals important**

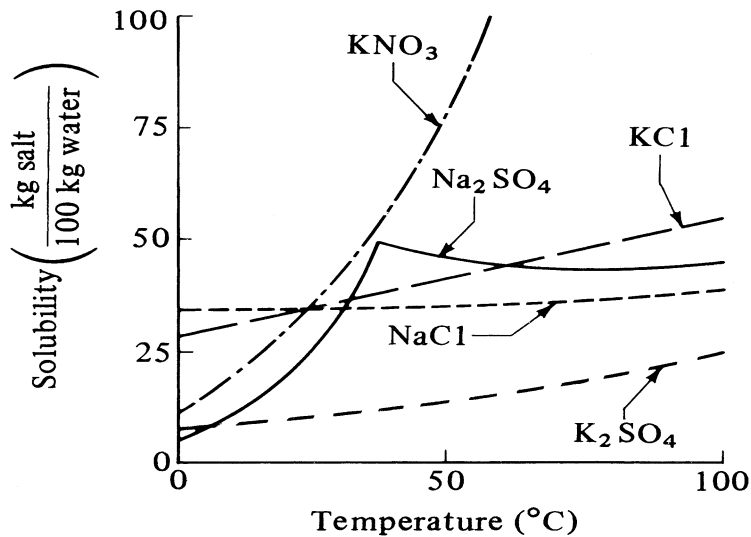
- **crystals - uniform in size**

- **formation of 1,4-naphthoquinone crystals from a liquid solution**

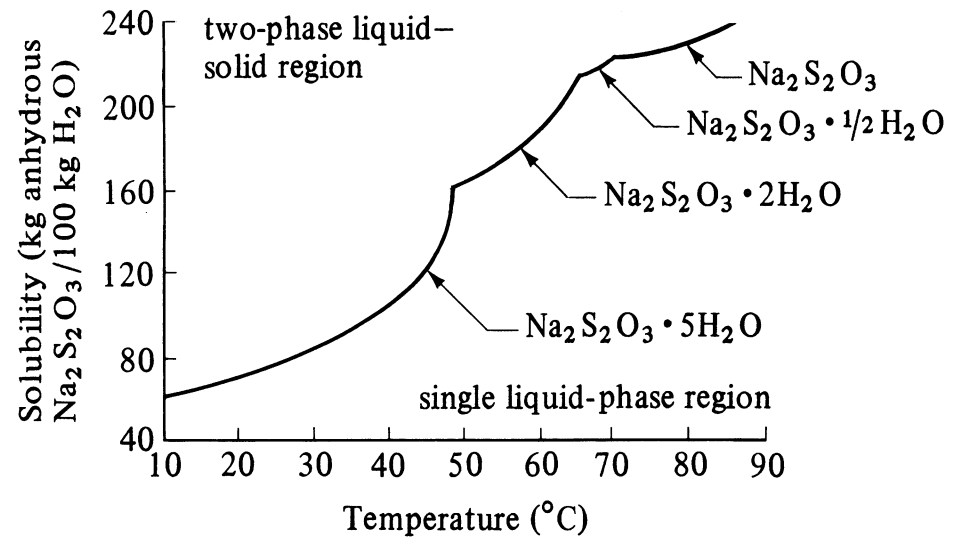
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# SOLUBILITY CURVE

- equilibrium is attained when the solution or mother liquor is saturated (represented by solubility curve)
- solubility dependent mainly on temperature
- solubilities of most salts increase slightly or markedly with temperature



Solubility curve for some typical salts in water



Solubility curve for sodium thiosulfate

# SOLID-LIQUID PHASE DIAGRAM

Saturation curve/line

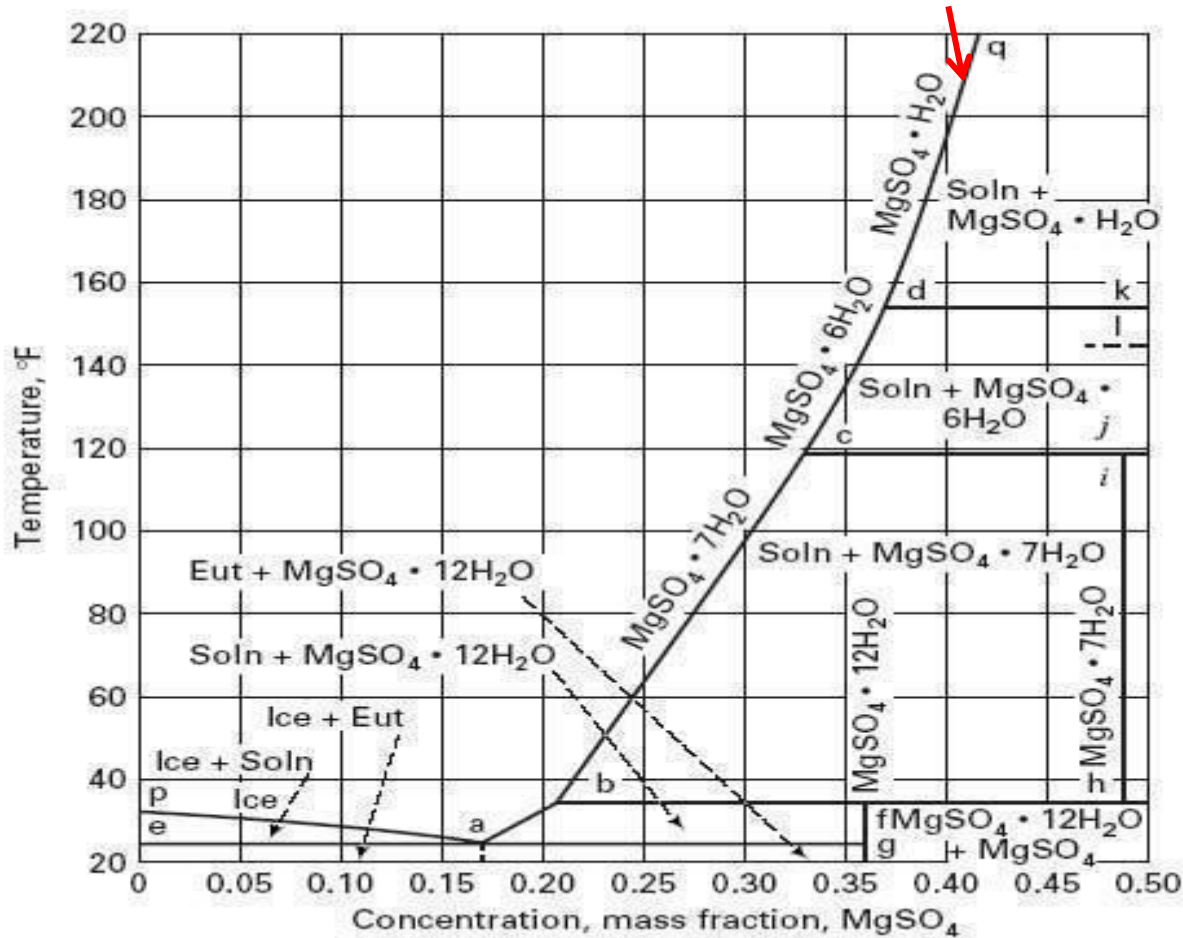


Figure 27.3-Solubility curve for the MgSO<sub>4</sub>-nH<sub>2</sub>O system at 1 atm

# YIELD & MATERIAL & HEAT BALANCES

- **yield** of crystals can be calculated by knowing:

initial concentration of solute

final temperature

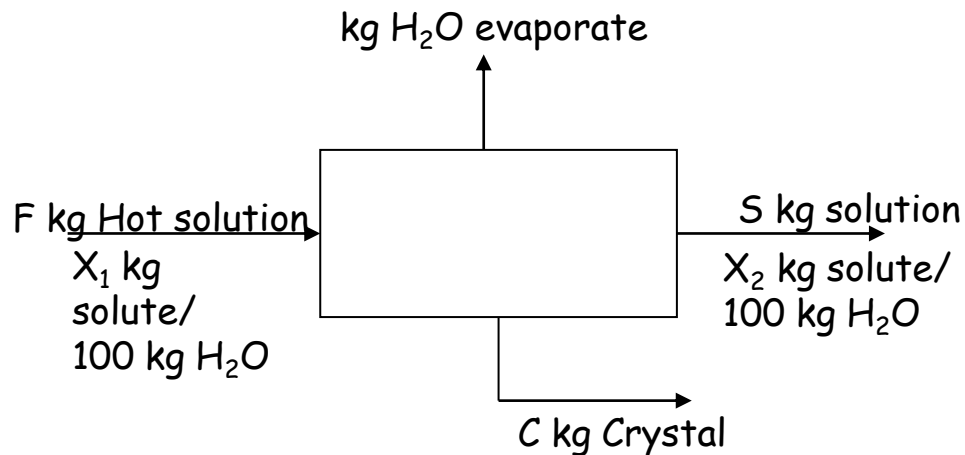
solubility at this temperature

- **material** balances

Mass balance :

Water balance : Input = Output

Solute balance : Input = Output



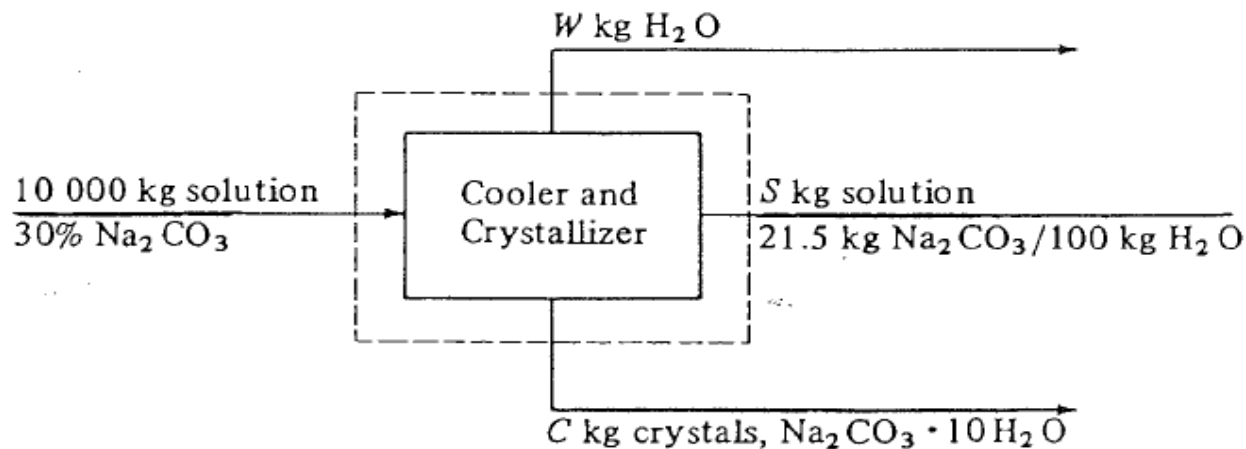
solute crystals are anhydrous - simple water & solute material balances

crystals are hydrated - some water in the solution is removed with crystals

## EXAMPLE 2

A salt solution weighing 10000 kg with 30 wt. %  $\text{Na}_2\text{CO}_3$  is cooled from 333K to 293K. The salt crystallizes as the decahydrate. What will be the yield of  $\text{Na}_2\text{CO}_3 \cdot 10\text{H}_2\text{O}$  crystals if the solubility is 21.5 kg anhydrous  $\text{Na}_2\text{CO}_3/100\text{kg}$  water?

- Assume that no water is evaporated.
- Assume that 3% of the total weight of the solution is lost by evaporation of water in cooling.





## EXAMPLE 3

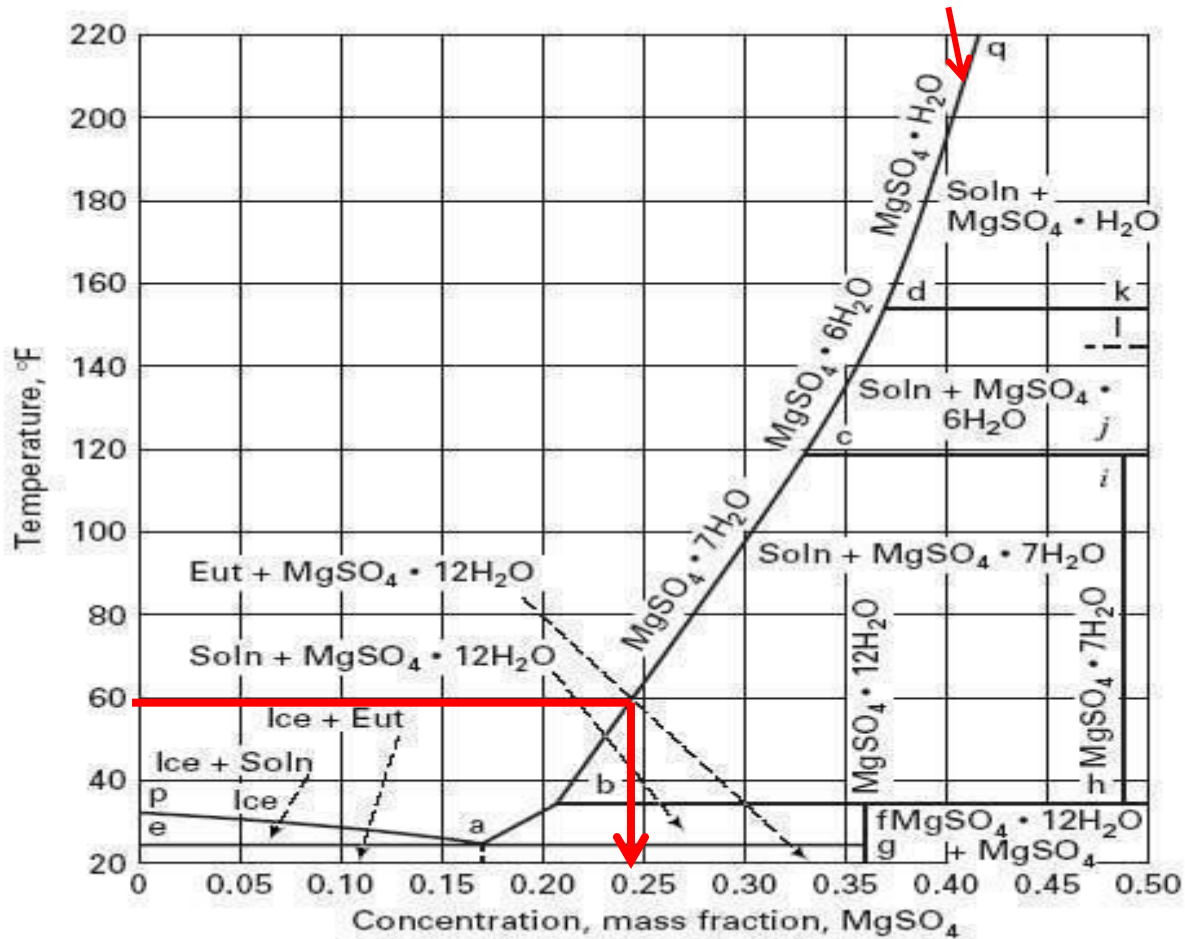
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**A solution consisting of 30 wt%  $\text{MgSO}_4$  and 70% water is cooled to 60°F. During cooling 5% of the total water in the system evaporates. How many kilograms of crystals are obtained per 1000 kg of the original mixture?**

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# SOLID-LIQUID PHASE DIAGRAM

Saturation curve/line



Solubility curve for the  $\text{MgSO}_4$ - $n\text{H}_2\text{O}$  system at 1 atm



## EXAMPLE 4

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A feed of solution of 2268 kg at 327.6 K (54.4°C) containing 48.2 kg  $\text{MgSO}_4$ /100 kg total water is cooled to 293.2 K (20°C), where  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$  crystals are removed. The solubility of the salt is 35.5 kg  $\text{MgSO}_4$ /100 kg total water. The average heat capacity of the feed solution can be assumed as 2.93 kJ/kg.K. The heat of solution at 291.2 K (18°C) is  $13.31 \times 10^3$  kJ/kg mol  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ .

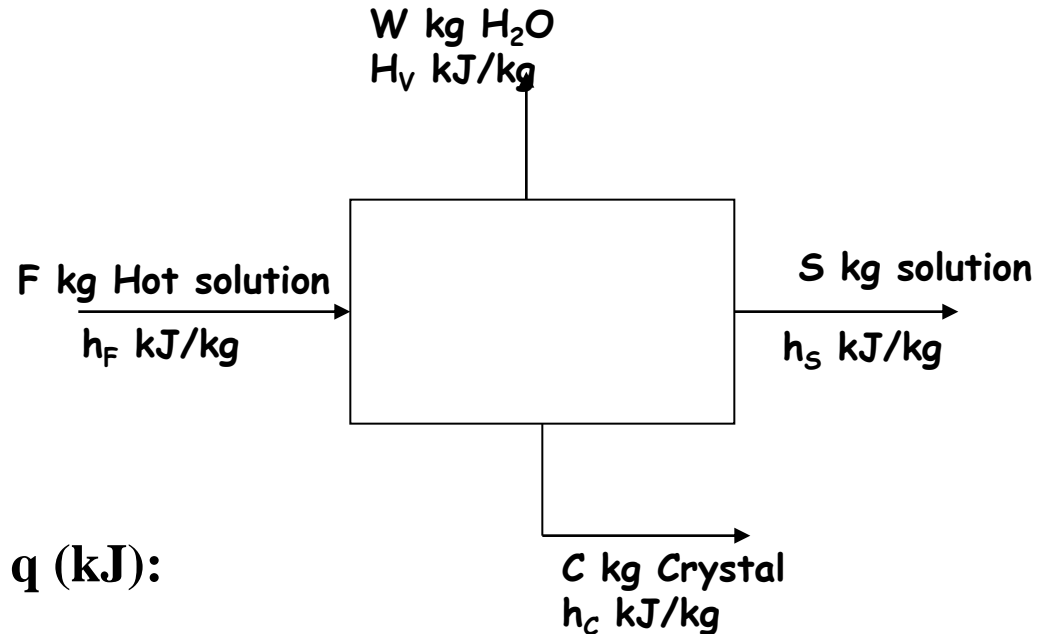
Calculate the yield of crystals.

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# HEAT BALANCES IN CRYSTALLIZATION

normally, crystallization is exothermic



Total heat absorbed,  $q$  (kJ):

When  $T_{\text{datum}} = 32^{\circ}\text{F} = 0^{\circ}\text{C}$ ,

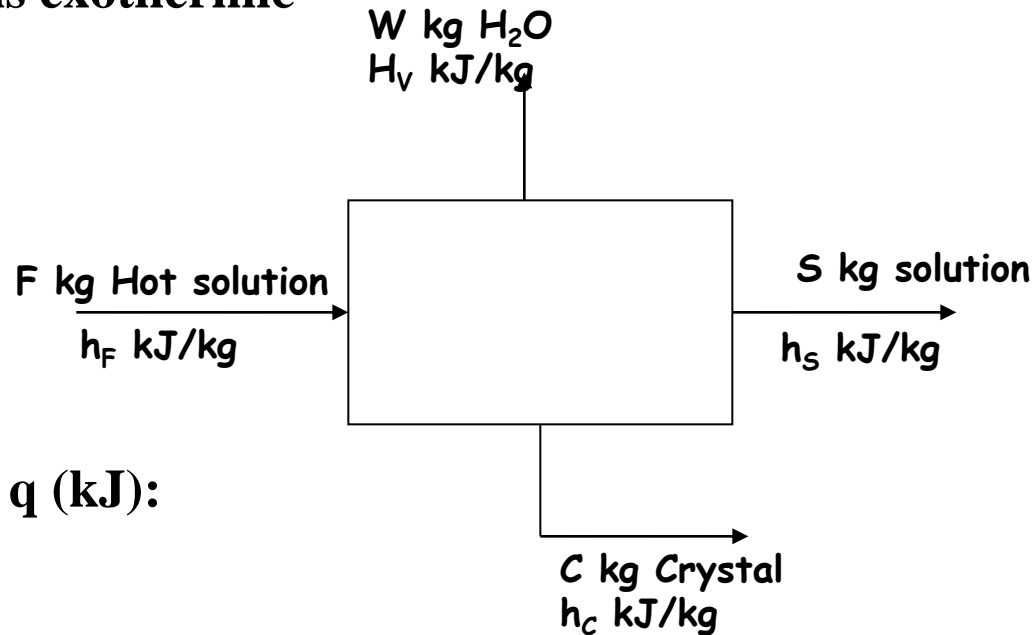
or

$$Fh_F + q = (S + C)h_M + WH_V$$

$$Fh_F + q = Sh_S + Ch_C + WH_V$$

# HEAT BALANCES IN CRYSTALLIZATION

normally, crystallization is exothermic



Total heat absorbed,  $q$  (kJ):

**When  $T_{\text{datum}} = T_{\text{equil./sat.}}$  ,** 
$$Fh_F + q = W\lambda + Ch_C = W\lambda + C\Delta H_{\text{crys}}^{\infty}$$

heat of crystallization,  $\Delta H_{\text{crys}} = -$  heat of solution at infinite dilution,  $\Delta H_{\text{soln}}^{\infty}$

Heat absorbed,  $q = +$ 've , Heat given off ,  $q = -$ 've



## EXAMPLE 4

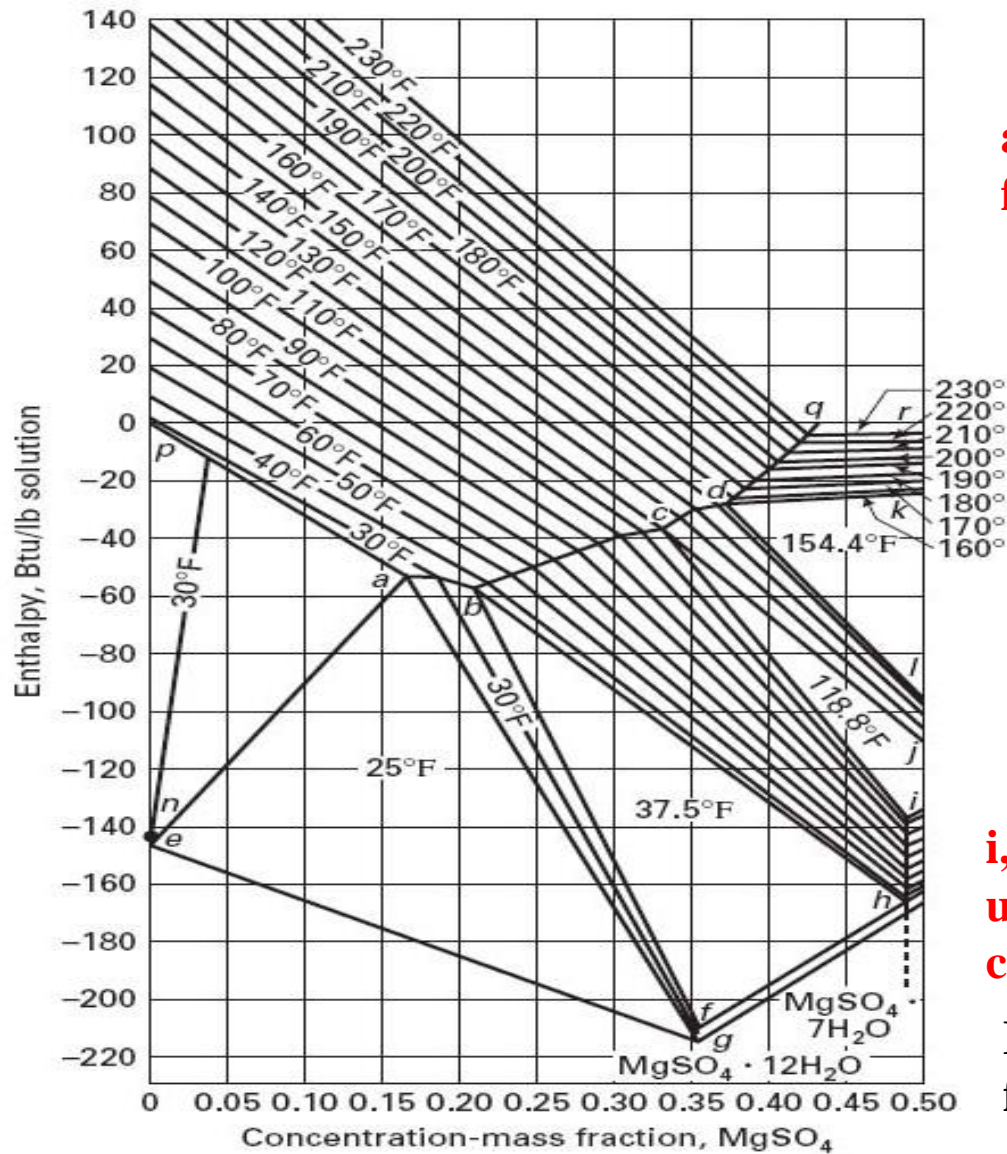
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Calculate the yield of crystals and **make a heat balance to determine the total heat absorbed/released,  $q$ , assuming that no water is vaporized.**

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# ENTHALPY-CONCENTRATION DIAGRAM



**a, b, c, d – saturation line, use to find enthalpy of solution**

**i, h – complete crystallization, use to find enthalpy of crystallization**

**Fig 27.4-Enthalpy-concentration diagram for the MgSO<sub>4</sub>-nH<sub>2</sub>O system at 1 atm**



## EXAMPLE 5

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**A 32.5% solution of  $\text{MgSO}_4$  at  $120^\circ\text{F}$  ( $48.9^\circ\text{C}$ ) is cooled, without appreciable evaporation to  $70^\circ\text{F}$  ( $21.1^\circ\text{C}$ ) in a batch-cooled crystallizer. How much heat must be removed from the solution per 100 Ib of the feed solution?**

**The average heat capacity of the feed solution is  $0.72 \text{ Btu/Ib } ^\circ\text{F}$  and the heat of solution at  $18^\circ\text{C}$  is  $23.2 \text{ Btu/Ib of } \text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ .**

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