

Chapter 8

Entropy

**A Measure of Disorder or
Randomness**

Entropy Definition and Change

DEFINE A PROPERTY **S** ENTROPY

$$\int_{1 \text{ rev}}^2 \frac{\delta Q}{T} = S_2 - S_1$$

$$\int_{2 \text{ irrev}}^1 \frac{\delta Q}{T} + S_2 - S_1 \leq 0$$

$$\int_{2 \text{ irrev}}^1 \frac{\delta Q}{T} + ds \leq 0$$

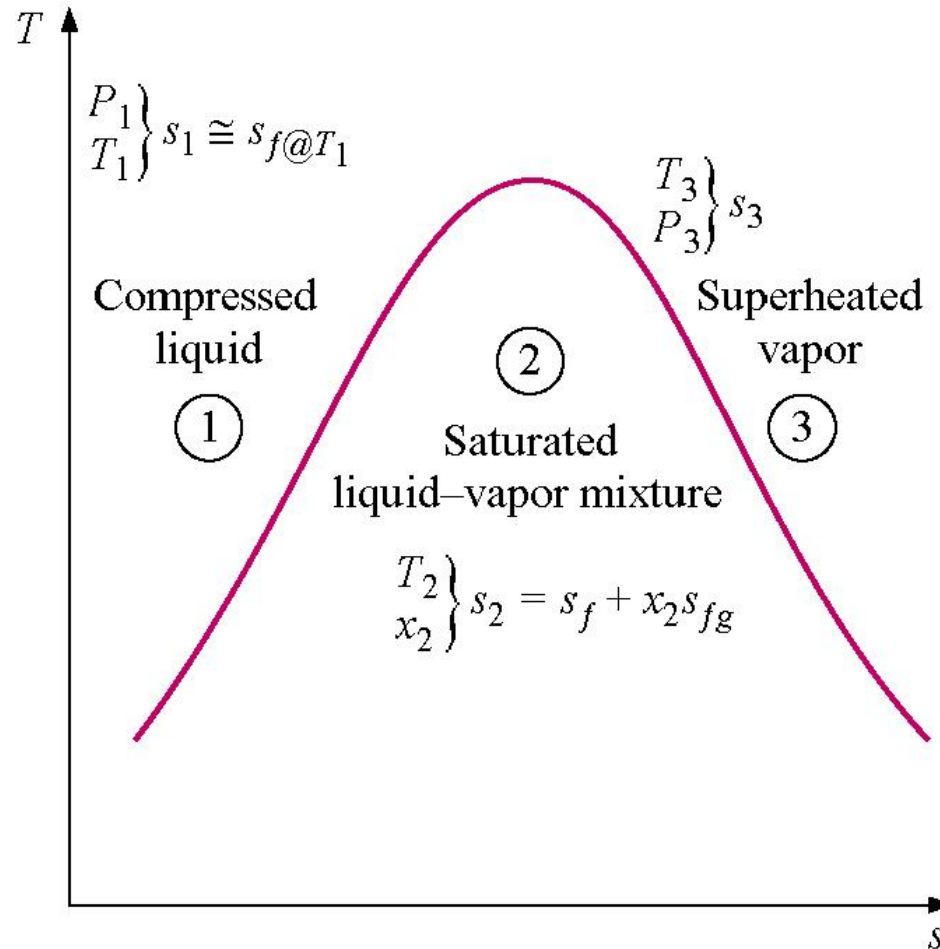
$$ds \geq \int_{2 \text{ irrev}}^1 \frac{\delta Q}{T}$$

$$ds \geq \int_{\text{irrev}} \frac{\delta Q}{T}$$

$$ds = \int_{\text{rev}} \frac{\delta Q}{T}$$

$$\delta Q = \int T ds$$

The temperature-entropy diagrams for water



Entropy for a Pure Substance

Values of specific entropy are given in tables of thermodynamic properties.

The tables are the same as for u , h and v

$$s = (1 - x)s_f + s_g$$

OR

$$s = s_f + xs_{fg}$$

Example 8-1

Find the entropy and/or temperature of steam at the following states:

P	T	Region	s kJ/(kg K)
5 MPa	120°C		
1 MPa	50°C		
1.8 MPa	400°C		
40 kPa		Quality, $x = 0.9$	
40 kPa			7.1794

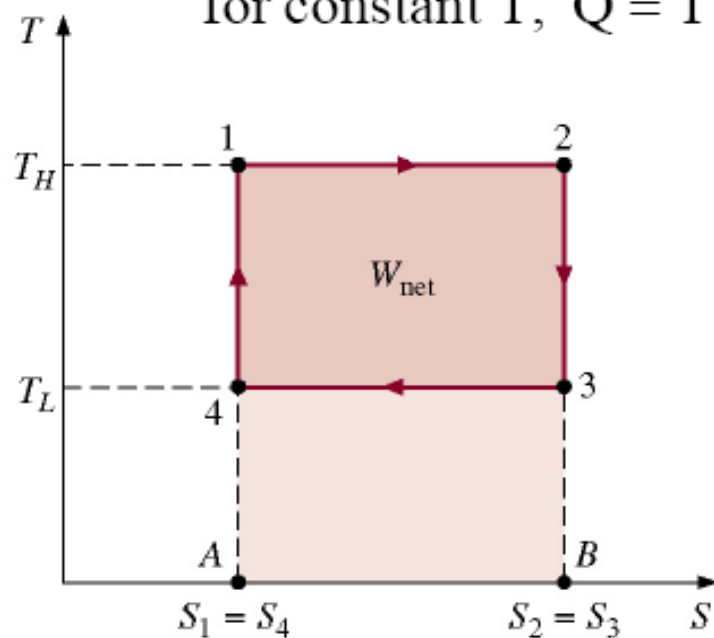
Answer to Example 8-1

P	T	Region	s kJ/kg·K
5 MPa	120°C	Compressed Liquid and in the table	1.5233
1 MPa	50°C	Compressed liquid but not in the table	$s = s_f$ at 50°C $= 0.7038$
1.8 MPa	400°C	Superheated	7.1794
40 kPa	$T = T_{\text{sat}}$ $= 75.87^\circ\text{C}$	Quality, $x = 0.9$ Saturated mixture	$s = s_f + x s_{fg}$ $= 7.0056$
40 kPa	$T = T_{\text{sat}}$ $= 75.87^\circ\text{C}$	$s_f < s < s_g$ at P Saturated mixture $X = (s - s_f) / s_{fg}$ $= 0.9262$	7.1794

Temperature Entropy Property Diagrams

$$dS = \int \frac{\delta Q}{T}$$

$$\text{for constant } T, Q = T \int dS = T_{\text{constant}} \Delta S$$



$$Q_{\text{in}} = T_H \Delta S$$

$$Q_{\text{out}} = T_L \Delta S$$

$$W_{\text{net}} = Q_{\text{in}} - Q_{\text{out}} = (T_H - T_L) \Delta S$$

The Thermodynamic Property Relation

From First Law for a closed system,

$$\partial Q - \partial W = dU + dKE + dPE$$

$$\partial Q - \partial W = dU$$

For reversible process,

$$\partial Q_{rev} = dU + \partial W_{rev}$$

$$TdS = dU + PdV$$

$$dU = TdS - PdV \quad (8.5)$$

$$du = Tds - PdV \quad (8.5)$$

From definition of enthalpy,

$$H = U + PV$$

Differential,

$$dH = dU + PdV + VdP$$

Replaced into Eq(8.5),

$$TdS = dH - VdP$$

OR

$$dH = TdS + VdP$$

Entropy Change for Solid and Liquid

$$du = Tds - Pdv$$

$$dh = Tds + vdP$$

For liquid and solid, v is almost negligible; $dv \approx 0$ for all process. If dP is small,

$$du = Tds$$

$$dh = Tds$$

From Eq.(5.17) for solid and liquid,

$$dh \approx du \approx CdT \quad (\text{no phase change})$$

And $C_p \approx C_v \approx C$

- So,

$$ds \approx C \frac{dT}{T}$$

- If C is constant,

$$\Delta s = s_2 - s_1 = C \ln \frac{T_2}{T_1}$$

8.20

Entropy Change for Ideal Gas

- From $du = Tds - Pdv$
- For ideal gas,

$$C_{vo} dT = Tds - \frac{RT}{v} dv$$

$$ds = C_{vo} \frac{dT}{T} + R \frac{dv}{v}$$

$$\Delta s = \int C_{vo} \frac{dT}{T} + R \ln \frac{v_2}{v_1} \quad 8.22$$

$$\Delta s = C_{vo} \ln \frac{T_2}{T_1} + R \ln \frac{v_2}{v_1}$$

- **From** $dh = Tds + vdP$
- **For ideal gas,**

$$C_{p_o} dT = Tds + RT \frac{dP}{P}$$

$$ds = C_{p_o} \frac{dT}{T} - R \frac{dP}{P}$$

$$\Delta s = \int C_{p_o} \frac{dT}{T} - R \ln \frac{P_2}{P_1}$$

$$\Delta s = C_{p_o} \ln \frac{T_2}{T_1} - R \ln \frac{P_2}{P_1}$$

Reversible, adiabatic process (isentropic)

For ideal gas which is isentropic ($ds = 0$)

$$du = Tds - Pdv$$

$$du = -Pdv$$

$$k = C_p/C_v \quad C_p = C_v + R$$

$$C_v = R/k-1$$

and

$$C_p = kR/k-1$$

$$T_2/T_1 = (P_2/P_1)^{(k-1)/k} = (v_1/v_2)^{k-1}$$

Entropy Generation

$$dS = \frac{\partial Q}{T} + \partial S_{gen} \quad (8.11)$$

where $\partial S_{gen} \geq 0$

∂S_{gen} is a entropy generation due to irreversibility of the process. It is a path function.

$\delta S_{gen} = 0$ For reversible process

$\delta S_{gen} > 0$ For irreversible process

From Eq. (8.11), the conclusion can be drawn,

dS_{sys}	Reason
Increased (+)	1. Heat is transferred into the system 2. Irreversible process
Decreased (-)	Heat is transferred from the system
Unchanged (0)	Adiabatic and reversible process

Entropy equation

$$dS = \frac{\partial Q}{T} + \partial S_{gen} \quad (8.11)$$

where $\partial S_{gen} \geq 0$

$$s_2 - s_1 = \frac{Q_2}{T_o} + S_{gen}$$

Normally we need to calculate ${}_1S_2$ (Sgen)